

# Corrosion Inhibition of Mild Steel in Aqueous Solutions using Nonionic Surfactants

A. S Fouda<sup>1</sup>

<sup>1</sup> Fac.Sci., Mansoura University, Egypt

*Received: 15 December 2013 Accepted: 1 January 2014 Published: 15 January 2014*

---

## Abstract

The inhibiting effect of nonionic surfactant of Tween- 20 and 60 on the corrosion of mild steel in 0.5 M HCl was studied by weight loss, potentiodynamic polarization, electrochemical impedance spectroscopy (EIS) and electrochemical frequency modulation (EFM).techniques The results show that inhibition efficiency increases with increasing the inhibitor concentration, while it decreases with increasing the temperature. The adsorption of Tweens on the mild steel surface obeys the Langmuir adsorption isotherm. The effect of temperature on the corrosion behavior of mild steel was also studied at four temperatures ranging from 25 to 55°C the thermodynamic parameters were calculated and discussed. The values of free energy of adsorption for investigated Tweens were calculated. It was found the adsorption process is spontaneous and increases, in the same direction as inhibition efficiency. Polarization curves show that Tween-20 and 60 is mixed-type inhibitors but the cathode is more polarized than the anode. The results obtained from chemical and electrochemical techniques are in good agreement.

---

**Index terms**— corrosion inhibition, mild steel, HCL, tween 20 and 60.

## 1 Introduction

Corrosion is a fundamental process playing an important role in economics and safety particularly for metals. The use of inhibitors is one of the most practical methods for protection against corrosion especially in acidic media [1]. Most Wellknown acid inhibitors are organic compounds containing nitrogen, sulfur, and oxygen atoms. Among them, surfactant inhibitors have many advantages such as high inhibition efficiency, low price, low toxicity, and easy production [2][3][4][5][6]. Ionic surfactants have been used for the corrosion inhibition of iron [7][8][9][10][11][12], copper [13], aluminum [14][15][16], and other metals [17,18] in different corroding media. The adsorption of the surfactant on the metal surface can markedly change the corrosionresisting property of the metal [19,20] and so the study of the relations between the adsorption and corrosion inhibition is of great important. Nonionic surfactants have shown a high inhibition efficiency for iron in both HCl [21, 22] and H<sub>2</sub>SO<sub>4</sub> [23] solutions. Nonionic surfactants were II.

## 2 Experimental Methods

### 3 a) Materials

Tests were performed on mild steel of the following composition (weight %):0.15-0.20 % C, 0.60-0.90 % Mn, 0.04 % P, 0.05 % S, and the remainder Fe b) Inhibitors Tween 20 and 60 obtained from Shanghai Chemical Reagent Company of China and used as received. Table ?? shows the molecular structure of the Tweens. It is obvious that Tweens are O-heterocyclic compounds. The main functional group is hydroxyl. The molecular weights of Tweens are also high because of a number of units CH<sub>2</sub> CH<sub>2</sub> O.

## 7 A) WEIGHT LOSS MEASUREMENTS

41 Table ?? : The names and molecular structures of the investigated Tweens c) Solutions

42 The aggressive solutions, 0.5 M HCl were prepared by dilution of analytical grade HCl (37%) with bi-distilled  
43 water. The concentration range of the inhibitors used was 20-120 ppm d) Gravimetric measurements Seven  
44 parallel mild steel sheets of  $2.5 \times 2.0 \times 0.06$  cm were abraded with emery paper (grade 320-500-800) and then  
45 washed with bidistilled water and acetone. After accurate weighing, the specimens were immersed in a 250 ml  
46 beaker, which contained 250 ml of HCl with and without addition of different concentrations of Tween-20 and  
47 60.

48 All the aggressive acid solutions were open to air. After 3 h, the specimens were taken out, washed, dried, and  
49 weighed accurately. The average weight loss of seven parallel mild steel sheets could be obtained. The inhibition  
50 efficiency (%IE) and the degree of surface coverage  $\theta$ , of Tween-20 and 60 for the corrosion of mild steel was  
51 calculated as follows [29], %IE =  $\theta \times 100 = [W^o - (W - W^o)] \times 100$ (1)

52 Where  $W^o$  and  $W$  are the values of the average weight loss without and with addition of the inhibitor,  
53 respectively.

### 54 4 e) Polarization measurements

55 Polarization experiments were carried out in a conventional three-electrode cell with a platinum counter electrode  
56 and a saturated calomel electrode (SCE) coupled to a fine Luggin capillary as the reference electrode. The working  
57 electrode was in the form of a square cut from mild steel embedded in epoxy resin of polytetrafluoroethylene  
58 (PTFE) so that the flat surface was the only surface in the electrode. The working surface area was  $1.0 \times 1.0$   
59 cm. Tafel polarization curves were obtained by changing the electrode potential automatically from -600 to +300  
60 mV at open circuit potential with a scan rate  $5 \text{ mVs}^{-1}$ . Stern-Geary method [30] used for the determination  
61 of corrosion current is performed by extrapolation of anodic and cathodic Tafel lines to a point which gives log  
62  $i_{\text{corr}}$  and the corresponding corrosion potential ( $E_{\text{corr}}$ ) for inhibitor free acid and for each concentration of  
63 inhibitor. Then  $i_{\text{corr}}$  was used for calculation of inhibition efficiency and surface coverage ( $\theta$ ) as below: % IE =  
64  $\theta \times 100 = [1 - (i_{\text{corr}}(\text{inh}) / i_{\text{corr}}(\text{free}))] \times 100$ (2)

65 Where  $i_{\text{corr}}(\text{free})$  and  $i_{\text{corr}}(\text{inh})$  are the corrosion current densities in the absence and presence of inhibitor,  
66 respectively.

67 Impedance measurements were carried out in frequency range from 100 kHz to 10 mHz with amplitude of  
68 5 mV peak-to-peak using ac signals at open circuit potential. The experimental impedance were analyzed and  
69 interpreted on the basis of the equivalent circuit. The main parameters deduced from the analysis of Nyquist  
70 diagram are the resistance of charge transfer  $R_{\text{ct}}$  (diameter of high frequency loop) and the capacity of double  
71 layer  $C_{\text{dl}}$  which is defined as:  $C_{\text{dl}} = 1 / (2 \pi f_{\text{max}} R_{\text{ct}})$ (3)

72 The inhibition efficiencies and the surface coverage ( $\theta$ ) obtained from the impedance measurements are defined  
73 by the following relation: IE % =  $\theta \times 100 = [1 - (R_{\text{ct}} / R_{\text{ct}}^o)] \times 100$ (4)

74 Where  $R_{\text{ct}}^o$  and  $R_{\text{ct}}$  are the charge transfer resistance in the absence and presence of inhibitor, respectively.

75 Electrochemical frequency modulation, EFM, was carried out using two frequencies 2 and 5 Hz. The base  
76 frequency was 0.1 Hz, so the waveform repeats after 1 s. The higher frequency must be at least two times the  
77 lower one. The higher frequency must also be sufficiently slow that the charging of the double layer does not  
78 contribute to the current response often; 10 Hz is a reasonable limit. The Intermodulation spectra contain current  
79 responses assigned for harmonical and intermodulation current peaks. The larger peaks were used to calculate  
80 the corrosion current density ( $i_{\text{corr}}$ ), the Tafel slopes ( $\beta_c$  and  $\beta_a$ ) and the causality factors CF-2& CF-3 [31].

81 The electrode potential was allowed to stabilize 30 min before starting the measurements. All the ex-  
82 periments were conducted at  $30 \pm 1^\circ\text{C}$ . Measurements were performed using Gamry Instrument Potentio-  
83 stat/Galvanostat/ZRA. This includes a Gamry framework system based on the ESA 400. Gamry applications  
84 include DC105 for corrosion measurements, EIS300 for electrochemical impedance spectroscopy and EFM 140 for  
85 electrochemical frequency modulation measurements along with a computer for collecting data. Echem Analyst  
86 5.58 software was used for plotting, graphing, and fitting data.

## 87 5 III.

## 88 6 Results and Discussion

### 89 7 a) Weight loss measurements

90 The weight loss-time curves of mild steel with the addition of tween 60 in 0.5 M HCl at various concentrations  
91 is shown in Fig. 1 as an example. The curves of Fig. 1 show that the weight loss values of mild steel in 0.5  
92 M HCl solution containing Tween 60 decrease as the concentration of the inhibitor increases; i.e., the corrosion  
93 inhibition strengthens with the nonionic surfactant concentration. This trend may result from the fact that the  
94 adsorption of surfactant on the mild steel increases with the increase of inhibitor concentration thus the mild steel  
95 surface is efficiently separated from the medium by the formation of a film on its surface [32]. Figure 2 shows the  
96 anodic and cathodic Tafel polarization curves for mild steel in 0.5 M HCl in the absence and presence of varying  
97 concentrations of tween 60 at  $25^\circ\text{C}$  as an example. The effect of temperature on the IE % for Tweens was studied  
98 using this technique. From Fig. 2, it is clear that both anodic metal dissolution and cathodic reduction reactions  
99 were inhibited when Tweens were added to 0.5 M HCl and this inhibition was more pronounced with increasing

inhibitor concentration. Tafel lines are shifted to more negative and more positive potentials with respect to the blank curve by increasing the concentration of the Tweens. This behavior indicates that the undertaken additives act as mixed type inhibitors [33,34]. The results show that the increase in inhibitor concentration leads to decrease the corrosion current density ( $i_{corr}$ ), but the Tafel slopes ( $\beta_a$  and  $\beta_c$ ) are approximately constant indicating that the retardation of the two reactions (cathodic hydrogen reduction and anodic metal dissolution) were affected without changing the dissolution mechanism [35][36][37][38] (Table 2). The effect of inhibitor concentration on the impedance behavior of mild steel in 0.5 M HCl solution at 25°C is presented in Fig. 1a. The curves show a similar type of Nyquist plots for mild steel in the presence of various concentrations of Tween 60. Similar curves were obtained for Tween 20 (not shown). The existence of single semi-circle showed the single charge transfer process during dissolution which is unaffected by the presence of inhibitor molecules. Deviations from perfect circular shape are often referred to the frequency dispersion of interfacial impedance which arises due to surface roughness, impurities, dislocations, grain boundaries, adsorption of inhibitors, and formation of porous layers and in homogenates of the electrode surface [39,40]. Inspections of the data reveal that each impedance diagram consists of a large capacitive loop with one capacitive time constant in the Bode-phase plots (Fig. 1b). The electrical equivalent circuit model is shown in Fig. 4. It used to analyze the obtained impedance data. The model consists of the solution resistance ( $R_s$ ), the charge-transfer resistance of the interfacial corrosion reaction ( $R_{ct}$ ) and the double layer capacitance ( $C_{dl}$ ). Excellent fit with this model was obtained with our experimental data. EIS data (Table 3) show that the  $R_{ct}$  values increases and the  $C_{dl}$  values decreases with increasing the inhibitor concentrations. This is due to the gradual replacement of water molecules by the adsorption of the inhibitor molecules on the metal surface, decreasing the extent of dissolution reaction. The high ( $R_{ct}$ ) values, are generally associated with slower corroding system [41,42].

The decrease in the  $C_{dl}$  can result from the decrease of the local dielectric constant and/or from the increase of thickness of the electrical double layer suggested that the inhibitor molecules function by adsorption at the metal/solution interface [43]. The % IE obtained from EIS measurements are close to those deduced from polarization measurements. The order of inhibition efficiency obtained from EIS measurements is as follows: Tween 20 > Tween 60. 4).

From Table 4, the corrosion current densities decrease by increasing the concentration of investigated compounds and the inhibition efficiencies increase by increasing investigated concentration of the investigated compounds. The causality factors in Table 4 are very close to theoretical values which according to EFM theory should guarantee the validity of Tafel slopes and corrosion current densities. Values of causality factors in Table 3 indicate that the measured data are of good quality. The standard values for CF-2 and CF-3 are 2.0 and 3.0, respectively. The deviation of causality factors from their ideal values might due to that the perturbation amplitude was too small or that the resolution of the frequency spectrum is not high enough also another possible explanation that the inhibitor is not performing very well. The obtained results showed good agreement of corrosion kinetic parameters obtained with the EFM, Tafel extrapolation and EIS methods. Organic molecules inhibit the corrosion process by the adsorption on metal surface. Theoretically, the adsorption process can be regarded as a single substitutional process in which an inhibitor molecule, I, in the aqueous phase substitutes an "x" adsorbed on the metal surface [44,45]

Where x is known as the size ratio and simply equals the number of adsorbed water molecules replaced by a single inhibitor molecule. The adsorption depends on the structure of the inhibitor, the type of the metal and the nature of its surface, the nature of the corrosion medium and its pH value, the temperature and the electrochemical potential of the metal-solution interface. Also, the adsorption provides information about the interaction among the adsorbed molecules themselves as well as their interaction with the metal surface.

The values of surface coverage,  $\theta$ , for different concentration of the studied compound at different temperatures have been used to explain the best isotherm to determine the adsorption process.

By far the results of investigated Tweens were best fitted by Langmuir adsorption isotherm. Figures 2 and 7 show the plotting of  $C/\theta$  against C at different temperatures for Tween 20 and 60, respectively. These plots gave straight lines with unit slope indicating that the adsorption of investigated Tweens on mild steel surface follows Langmuir adsorption isotherm [46]:  $C/\theta = 1/K + C$  (6)

Where C is the concentration of inhibitor,  $\theta$  the fractional surface coverage and K is the adsorption equilibrium constant related to the free energy of adsorption  $\Delta G^{\circ}_{ads}$  as [47].  $K = 1/55.5 \exp(-\Delta G^{\circ}_{ads}/RT)$  (7) Where R is the universal gas constant, T is the absolute temperature. The value 55.5 is the concentration of water on the metal surface in mol/L.

The calculated  $\Delta G^{\circ}_{ads}$  values, using Eq. (6), were also given in Table 5.  $\Delta G^{\circ}_{ads}$  is expressed in kJ mol<sup>-1</sup> of Org ads. The negative values of  $\Delta G^{\circ}_{ads}$  ensure the spontaneity of the adsorption process and the stability of the adsorbed layer on the mild steel surface. It is well known that values of  $\Delta G^{\circ}_{ads}$  of the order of 40 kJ mol<sup>-1</sup> or higher involve charge sharing or transfer from the inhibitor molecules to metal surface to form coordinate type of bond (chemisorption); lower indicate a physisorption [48,49].

The calculated  $\Delta G^{\circ}_{ads}$  values are in the range 38.6-41.9 kJ mol<sup>-1</sup> indicates, therefore, that the adsorption mechanism of the investigated compounds on mild steel in 0.5 M HCl solution is a simple physical adsorption. The higher negative values of  $\Delta G^{\circ}_{ads}$  indicate that these inhibitors are strongly adsorbed on the mild steel surface. Moreover,  $|\Delta G^{\circ}_{ads}|$  of investigated compounds decreases in the order Tween 60 > Tween 20. This is in good agreement with the ranking of inhibitors efficiency obtained from the different investigated techniques. The

higher values of K for tween 20 and 60 are  $1.04 \times 10^5$ ,  $1.71 \times 10^5$  M<sup>-1</sup> respectively; indicate stronger adsorption on the mild steel surface in 0.5 M HCl solution. The strong interaction of inhibitor with mild steel surface can be attributed to the presence of O atoms and  $\pi$ -electrons in the inhibitor molecules. Lagrenee et al [50] have reported that the higher K value ( $> 100$  M<sup>-1</sup>), the stronger and more stable adsorbed layer is forming which results in the higher inhibition efficiency. Thermodynamic parameters are important in studying the inhibitive mechanism. The values of enthalpy of adsorption,  $\Delta H^\circ_{ads}$  and entropy of adsorption,  $\Delta S^\circ_{ads}$  were obtained from the plot of  $\Delta G^\circ_{ads}$  versus T and from the basic thermodynamic equation (8):  $\Delta G^\circ_{ads} = \Delta H^\circ_{ads} - T \Delta S^\circ_{ads}$  (8)

$\Delta H^\circ_{ads}$  obtained were -10.9 and -18.9 kJ mol<sup>-1</sup> for Tween 20 and 60 respectively. The negative sign of  $\Delta H^\circ_{ads}$  obtained indicates the exothermic nature of the corrosion process [51] which indicates that % IE decreases with increasing the temperature. Generally, an exothermic process signifies either physisorption or chemisorption while endothermic process is attributable unequivocally to chemisorption [52]. In an exothermic process, physisorption is distinguished from chemisorption by considering the absolute value of a physisorption process is lower than 42 kJ mol<sup>-1</sup> while the adsorption heat of a chemisorption process approaches 100 kJ mol<sup>-1</sup> [53]. In the present case, the absolute value of the heat of adsorption is lower than 42 kJ mol<sup>-1</sup> approaching the typical value of physisorption. The values obtained for  $\Delta S^\circ_{ads}$  were 90 and 70 J mol<sup>-1</sup> K<sup>-1</sup> for Tween 20 and 60 respectively. The negative values of  $\Delta S^\circ_{ads}$  mean that the process of adsorption is accompanied by decrease in entropy. It might be explained as follows: before the adsorption of Tweens onto the mild steel surface, the chaotic degree of mild steel surface was high, but when inhibitor molecules were orderly adsorbed onto the mild steel surface, as a result, a decrease in entropy [54].

## 8 g) Effect of temperature

The effect of temperature on the rate of corrosion of mild steel in 0.5 M HCl containing different concentration from tween 20 or tween 60 was tested by potentiodynamic polarization measurements over a temperature range from 25 to 55 °C.

The effect of increasing temperature on the corrosion rate ( $i_{corr}$ ) and IE obtained from potentiodynamic polarization measurements.

The results revealed that, on the increasing solution temperature there is an increase of  $i_{corr}$  while IE decrease for all compound used. The activation energy ( $E^*_a$ ) of the corrosion process was calculated using Arrhenius equation:  $k = A \exp(-E^*_a / RT)$  (9)

Where k is the rate of corrosion, A is the Arrhenius constant, R is the gas constant and T is the absolute temperature.

Figure ?? present the Arrhenius plot in the presence of 40 ppm from investigated Tweens.  $E^*_a$  values determined from the slopes of these linear plots are ??1.8, 31.3 and 35.1 kJ mol<sup>-1</sup> for blank, tween 20 and tween 60 respectively. The linear regression ( $R^2$ ) is close to 1 which indicates that the corrosion of mild steel in 0.5 M HCl solution can be elucidated using the kinetic model. The values of  $E^*_a$  for inhibited solution is higher than that for uninhibited solution, suggesting that dissolution of mild steel is slow in the presence of tween and can be interpreted as due to physical adsorption [55]. It is known from Eq. 6 that the higher  $E^*_a$  values lead to the lower corrosion rate. This is due to the formation of a film on the mild steel surface serving as an energy barrier for the mild steel corrosion [56].

Enthalpy and entropy of activation ( $\Delta H^\ddagger$ ,  $\Delta S^\ddagger$ ) of the corrosion process were calculated from the transition state theory: Where h is Planck's constant and N is Avogadro's number. A plot of  $\log(i_{corr} / T)$  vs.  $1/T$  for mild steel in 0.5 M HCl at 80 ppm from investigated compounds, gives straight lines as shown in Figure ???. Values of  $\Delta H^\ddagger$  are, 8.5, 12, 14.2 kJ mol<sup>-1</sup> for blank, tween 20 and tween 60, respectively and these values are positive. This indicates that the corrosion process is an endothermic one. The entropy of activation is large and negative and in the range 97.3 to 110.9 Jmol<sup>-1</sup> K<sup>-1</sup>. This implies that the activated complex represents association rather than dissociation step, indicating that a decrease in disorder takes place, going from reactants to the activated complex [52]. In general, inhibition of different tween compounds depends on their structures. The inhibition efficiency increases in the following order: T 20 < T 60. ( $i_{corr}$ ) =  $(RT / Nh) \exp(\Delta S^\ddagger / R) \exp(-\Delta H^\ddagger / RT)$  (10)

This sequence reflects the effect of type of the fatty acid included in the tween formula, on their inhibitive action, since all tween compounds are mainly polyoxyethylene sorbitane combined with alkyl chain of different fatty acids which determine the tween number. Now, one can rewrite the above sequence, according the alkyl chain as following. Laurate (C12) < stearate (C18)

This new sequence illustrates the effects of both hydrocarbon length and presence of a double bond in the inhibitor structure. Thus, the inhibition efficiency increases as the number of carbon atoms in the alkyl chain increases.

## 9 IV.

## 10 Conclusions

It was found that the percentage inhibition efficiency depends on the concentration, temperature and chemical structure of Tweens and the inhibition efficiency is in the order: Tween 60 > Tween 20. The inhibition efficiency

223 increases as the length of the tween hydrocarbon chain is increased. Polarization curves demonstrate that the  
 224 examined Tweens behave as mixed type inhibitors. The results of EIS indicate that the double layer capacitance  
 225 decreases with respect to the blank solution when these inhibitors are added; this fact may be explained on  
 226 the basis of adsorption of these inhibitors on mild steel surface. The adsorption of investigated Tweens on  
 227 mild steel surface in HCl solution follows Langmuir adsorption isotherm. The negative values of  $\Delta G^{\circ}$  ads  
 228 show the spontaneity of the adsorption of Tweens on mild steel surface. The percentage inhibition efficiency of  
 229 Tweens obtained from the weight loss, potentiodynamic polarization curves, EIS and EFM techniques are in good  
 agreement.<sup>1</sup>



Figure 1: Figure 1 :

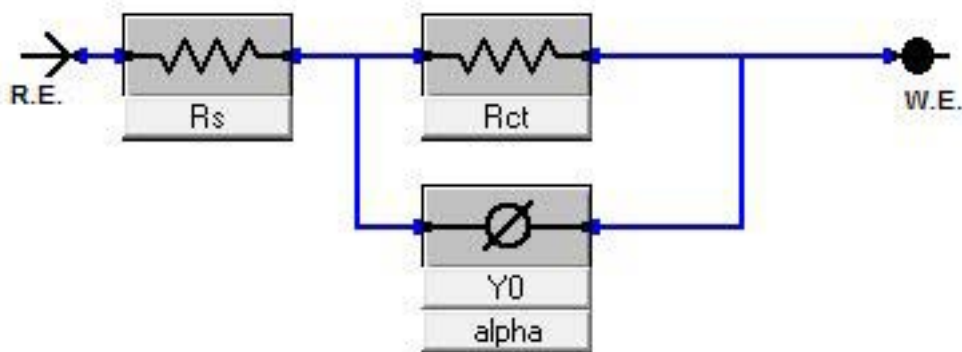


Figure 2: Figure 2 :

230

<sup>1</sup>© 2014 Global Journals Inc. (US)

34

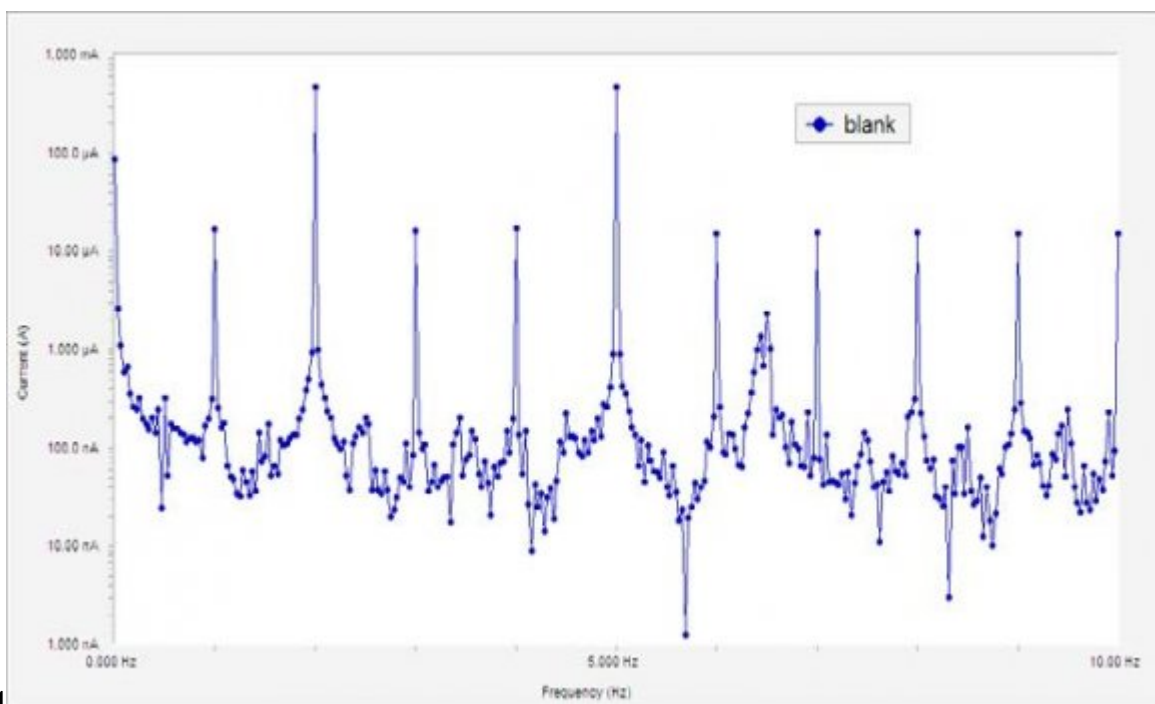


Figure 3: Figure 3 :Figure 4 :

5

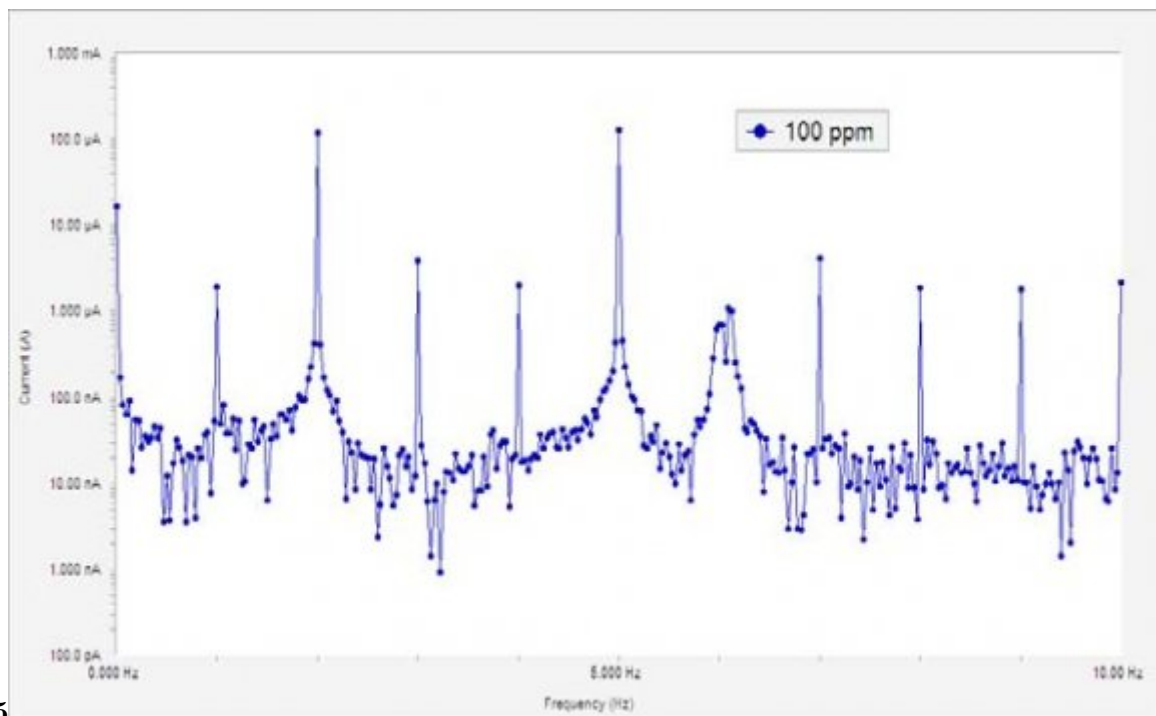
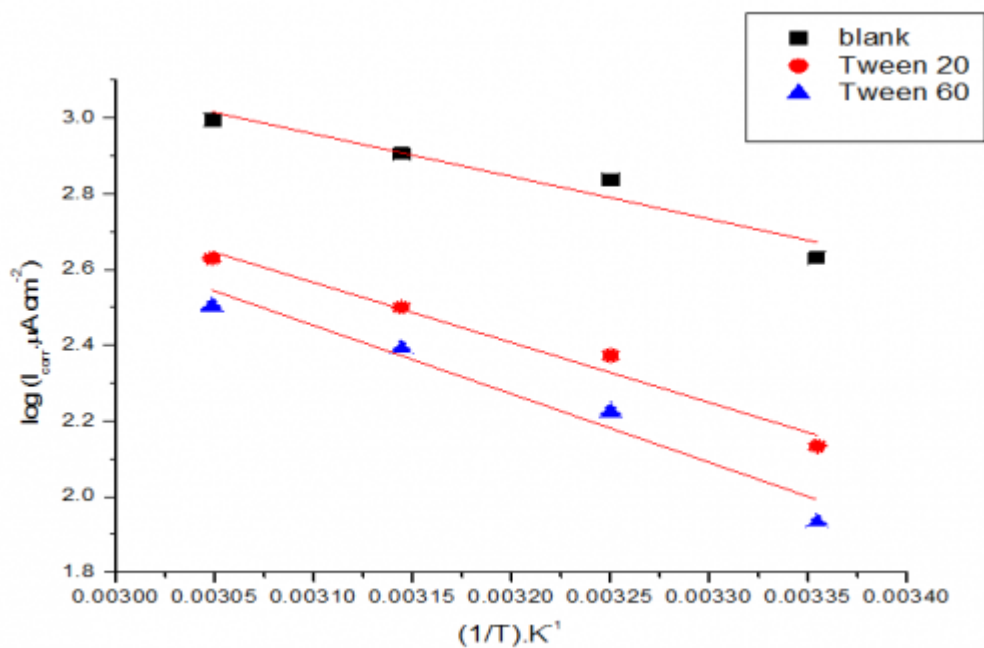
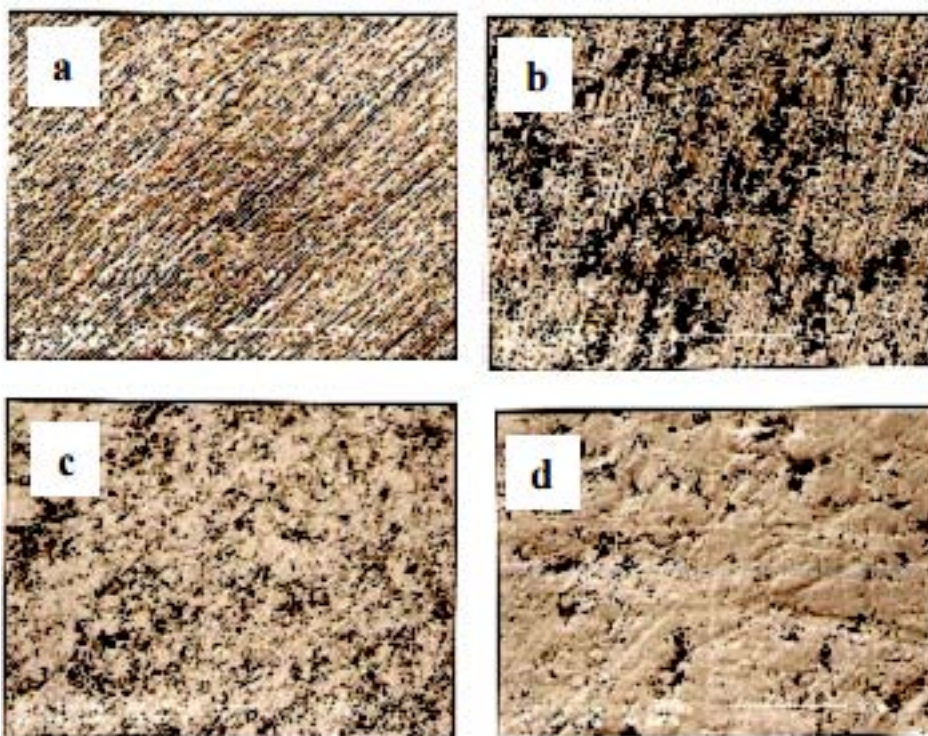


Figure 4: Figure 5 :



667

Figure 5: Figure 6 .Figure 6 :Figure 7 :



89

Figure 6: Figure 8 :Figure 9 :

2

Comp. Conc., ppm	-E <sub>corr</sub> mV vs SCE	i <sub>corr</sub> vs cm <sup>-2</sup>	i <sub>corr</sub> , μA	-η <sub>c</sub> , mVdec ?1	η <sub>a</sub> , mVdec ?1	η <sub>”</sub>	IE%	C.R., μm y <sup>-1</sup>
Blank 0.0	484		425.6	118	89	0.000	00.0	4940
20	486		162.2	104	79	0.619	61.9	1883
Tween 40 60	486 477		157.9 141.0	106 103	82 73	0.629 0.669	63.0 66.9	1833 1637
20 80 100	478 485		136.0 115.2	106 97	80 75	0.680 0.729	68.0 72.9	1579 1337
120	474		103.7	105	70	0.756	75.6	1204
20	457		115.3	106	69	0.729	73.0	1339
Tween 40 60	455 450		98.91 91.8	103 107	67 69	0.768 0.784	76.8 78.4	1148 1066
60 100	447		85.56	105	65	0.799	80.0	993
120	452		84.12	104	69	0.802	80.2	976

Figure 7: Table 2 :

3

at 25°C

Figure 8: Table 3 :

XIV  
Is-  
sue  
III  
Ver-  
sion  
I  
( )  
C  
Vol-  
ume

Global Comp. of various concentrations of tweens in 0.5 M HCl at 25 ° C ? CF-3 CF-2 ? a , mVdec ?1  
Jour- Blank M 6 3  
nal Tween B 00  
of 20 7 2 B  
Re- Tween 20 8 1  
searched 60 B 40  
in 9 0 B  
En- 60 9 9  
gi- B 80  
neer- 1 0 8  
ing B 100  
1 1 7  
B 20  
1 2 6  
B 40  
1 3 5  
B 60  
1 4 4  
B 80

1 5 2 B 104.9

1 1 1 1 1  
5 5 4 4 4  
1 0 9 8 7  
B B B B B  
92 1031.82.90.769

Figure 9: Table 4 :

Year 2014  
19  
XIV Issue III Version I  
( ) C Volume  
Journal of Researches in Engineering  
Global  
© 2014 Global Journals Inc. (US)

Figure 10:



- 231 [Hameed] , R S Hameed .
- 232 [Parr] , R G Parr .
- 233 [Benalli] , O Benalli .
- 234 [Epelboin] , I Epelboin .
- 235 [Lagreneee] , M Lagreneee .
- 236 [Mayer et al. ()] , J C Mayer , K Tuttner , W J Lorenz . *Electrochim. Acta* 1983. p. 171.
- 237 [Osman and Shalaby ()] , M M Osman , M N Shalaby . *Anti-Corros. Meth. Mater* 1997. 44.
- 238 [hysicochem. Eng. Aspects ()] , *hysicochem. Eng. Aspects* 2008. p. .
- 239 [Parr; R and Pearson ()] ‘Absolute hardness: companion parameter to absolute electronegativity’. R G G Parr;  
240 R , Pearson . *J. Am. Chem. Soc* 1983. 105 p. .
- 241 [Solmaz et al.] ‘Adsorption and corrosion inhibitive properties of 2-amino-5-mercapto-1,3,4-thiadiazole on mild  
242 steel in hydrochloric acid media’. R Solmaz , G Karda , B Yazici , M Erbil . *Colloids Surf.A*
- 243 [Lipkowski Ross (ed.) ()] *Adsorption of Molecules at Metal Electrodes*, J Lipkowski, P N Ross (ed.) (New York)  
244 1992. VCH.
- 245 [Algaber et al. ()] A S Algaber , E M El-Nemma , M M Saleh . *Effect of octylphenol polyethylene oxide on the*  
246 *corrosion inhibition of steel in 0.5 M H<sub>2</sub>SO<sub>4</sub>*, 2004. 86 p. .
- 247 [Branzoi et al. ()] ‘Aluminium corrosion in hydrochloric acid solutions and the effect of some organic inhibitors’.  
248 V Branzoi , F Golgovici , F Branzoi . *Mater. Chem. Phys* 2002. 78 p. .
- 249 [Moretti et al. ()] ‘An investigation of some Schiff bases as corrosion inhibitors for austenitic chromium-nickel  
250 steel in H<sub>2</sub>SO<sub>4</sub>’. G Moretti , G Quartanone , A Tassan , A Zingales . *Werkst. Korros* 1994. 45 p. .
- 251 [Benabdellah et al. ()] M Benabdellah , R Touzan , A Aouniti , A S Dafali , S El-Kadiri , B Hommouti , M  
252 Benkaddour . *Inhibitive action of some bipyrazolic compounds on the corrosion of steel in 1 M HCl: Part I:*  
253 *Electrochemical study*, 2007. 105 p. .
- 254 [Raeissi and Golozar ()] ‘Benzimidazole and its derivatives as corrosion inhibitors for mild steel in 1M HCl  
255 solution’. J , Aljourani K Raeissi , M A Golozar . *Corros. Sci* 2009. 51 p. .
- 256 [Banerjee and Malhotra ()] ‘Contribution to adsorption of aromatic amines on mild steel surface from HCl  
257 solutions by impedance, UV, and Raman spectroscopy’. G Banerjee , S N Malhotra . *Corrosion-NACE* 1992.  
258 48 p. .
- 259 [Arab and Noor ()] ‘Corrosion behavior of a Mg alloy AE42 subjected to friction stir processing’. S T Arab , E  
260 A Noor . *Corrosion-NACE* 1993. 49 p. .
- 261 [Abd El Rehim et al. ()] ‘Corrosion inhibition of aluminum by 1,1(lauryl amido)propyl ammonium chloride in  
262 HCl solution’. S S Abd El Rehim , H H Hassan , M A Amin . *Mater. Chem. Phys* 2001. 70 p. .
- 263 [Amar et al. ()] ‘Corrosion inhibition of Armco iron by 2-mercaptobenzimidazole in sodium chloride 3% media’.  
264 H Amar , Tounsi , Makayssi , Derja , Benzakour , Outzourhit . *Corros.Sci* 2007. 49 p. .
- 265 [Osman et al. ()] ‘Corrosion inhibition of benzyl triethanol ammonium chloride and its ethoxylate on steel in  
266 sulphuric acid solution’. M M Osman , A M Omar , A M Al-Sabagh . *Mater.Chem. Phys* 1997. 50 p. .
- 267 [Migahed et al. ()] ‘Corrosion inhibition of mild steel in 1M sulfuric acid solution using anionic surfactant’. M A  
268 Migahed , E M S Azzam , A M Al-Sabagh . *Mater. Chem. Phys* 2004. 85 p. .
- 269 [Abdallah and El-Etre ()] ‘Corrosion inhibition of nickel in sulfuric acid using tween surfactants’. M Abdallah ,  
270 A Y El-Etre . *Port. Electrochim. Acta* 2003. 21 p. .
- 271 [Szlarska-Smialowska ()] ‘Crevice corrosion of stainless steels in sodium chloride solution’. Z Szlarska-Smialowska  
272 . *Corros. Sci* 1978. 18 p. .
- 273 [Mernari et al. ()] ‘Crevice corrosion of stainless steels in sodium chloride solution’. B Mernari , M Bouanis , M  
274 Traisnel , F Bentiss . *Corros. Sci* 2002. 44 p. .
- 275 [Damaskin et al. ()] B B Damaskin , O A Petrii , V V Batrakov . *Adsorption of Organic compounds on Electrodes*,  
276 (New York) 1971. Plenum Press.
- 277 [Cahskan and Bilgic ()] ‘Effect of iodide ions on the synergistic inhibition of the corrosion of manganese-14 steel  
278 in acidic media’. N Cahskan , S Bilgic . *Appl. Surf. Sci* 2000. 153 p. .
- 279 [Mu et al. ()] ‘Effect of metallic cations on corrosion inhibition of an anionic surfactant for mild steel’. G N Mu  
280 , T P Zhao , M Liu , T Gu . *Corrosion* 1996. 52 p. .
- 281 [Villamil et al. ()] ‘Effect of sodium dodecylsulfate on copper corrosion in sulfuric acid media in the absence and  
282 presence of benzotriazole’. R F V Villamil , P Corio , J C Rubim , M L Siliva Agostinho . *J. Electroanal.*  
283 *Chem* 1999. 472 p. .

## 10 CONCLUSIONS

---

- 284 [El-Sherbiny ()] 'Effect of some ethoxylated fatty acids on the corrosion behavior of mild steel in sulphuric acid  
285 solution'. E F El-Sherbiny . *Mater. Chem. Phys* 1999. 60 p. .
- 286 [Guo et al. ()] 'Effects of SDS and some alcohols on the inhibition efficiency of corrosion for nickel'. R Guo , T  
287 Liu , X Wei . *Colloids Surf. A* 2002. 209 p. .
- 288 [Migahed et al. ()] 'Efficiency of some non ionic surfactants based on tolyl triazole as corrosion inhibitors for oil  
289 tubing steel during production process'. M A Migahed , M Abd-El-Raouf , A Misbah , A Marei , S Mahmoud  
290 . *Elixir Corrosion* 2012. 53 p. .
- 291 [Moussa and El-Far ()] 'El-Shafei, he use of water-soluble hydrazones as inhibitors for the corrosion of C-steel in  
292 acidic medium'. M N H Moussa , A A El-Far , AA . *Mater. Chem. Phys* 2007. 105 p. .
- 293 [Migahed et al. ()] 'Electrochemical behaviour of carbon steel in acid chloride solution in the presence of dodecyl  
294 cysteine hydrochloride self-assembled on gold nanoparticles'. M Migahed , E M Azzam , S M I Morsy .  
295 *Corros.Sci* 2009. 51 p. .
- 296 [Bosch et al. ()] *Electrochemical Frequency Modulation: A New Electrochemical Technique for Online Corrosion*  
297 *Monitoring Corrosion*, R W J Bosch , W F Hubrecht , B C Bogaerts , Syrett . 2001. 57 p. .
- 298 [Larabi et al. ()] 'Electrochemical, theoretical and XPS studies of 2-mercapto-1-methylimidazole adsorption on  
299 carbon steel in 1 M HClO<sub>4</sub>'. L Larabi , M Traisnel , L Gengembra , Y Harek . *Appl. Surf. Sci* 2007. 253 p. .
- 300 [Donnelly and Levy ()] 'Electronegativity: The density functional viewpoint'. D A Donnelly , M M Levy . *J.*  
301 *Chem. Phys* 1978. 68 p. .
- 302 [Hajjaji et al. ()] N Hajjaji , I Ricco , A Srhiri , A Lattes , M Soufiaoui , A Benbachir . *effect of N-alkylbetaines*  
303 *on the corrosion of iron in 1 M HCl solution*, 1993. 49 p. .
- 304 [Xianghong et al. ()] 'Inhibition effect of nonionic surfactant on the corrosion of cold rolled steel in hydrochloric  
305 acid'. Li Xianghong , Deng Shuduan , Mu Guannan , Fu Hui , Yang Fazhong . *Corros.Sci* 2008. 50 (2) p. .
- 306 [Ashassi-Sorkhabi and Ghalebsaz-Jeddi ()] 'Inhibition effect of polyethylene glycol on the corrosion of carbon  
307 steel in sulphuric acid'. H Ashassi-Sorkhabi , N Ghalebsaz-Jeddi . *Mater.Chem.Phys* 2005. 92 p. .
- 308 [El-Etre ()] 'Inhibition of aluminum corrosion using Opuntia extract'. A Y El-Etre . *Corros. Sci* 2003. 45 p. .
- 309 [Luo et al. ()] 'Inhibition of mild steel corrosion by sodium dodecyl benzene sulfonate and sodium oleate in acidic  
310 solutions'. H Luo , Y C Guan , K N Han . *Corrosion* 1998. 54 p. .
- 311 [Ismail; F et al. ()] 'New non-ionic polymeric surfactants as corrosion inhibitors for the C-Steel alloy in hy-  
312 drochloric acid corrosive medium'. O M M Ismail; F , R Eissa , Ghanem . *Der Chemica Sinica* 2012. 3 (1) p.  
313 .
- 314 [Masroor and Mobin ()] 'Non-ionic surfactant as corrosion inhibitor for aluminium in 1 M HCl and synergistic  
315 influence of gemini surfactant'. Sheerin Masroor , Mohammad Mobin . *Chem Sci Rev. Lett* 2014. 3 (11S) p. .
- 316 [Fouda et al. ()] 'Pyrazolone derivatives as corrosion inhibitors for Csteel in hydrochloric acid solution'. A S  
317 Fouda , A A Al-Sarawy , E E El-Katori . *Desalination* 2006. 201 p. .
- 318 [Elachouri et al. ()] 'Some Nonionic Surfactants as Inhibitors of the Corrosion of Iron in Acid Chloride Solutions'.  
319 M Elachouri , M S Hajji , M Salem , S Kertit , J Aride , R Coudert , E Essassi . *Corrosion* 1996. 52 p. .
- 320 [Elachour et al. ()] 'Some Nonionic surfactants as inhibitors of the corrosion of iron in acid chloride solutions'.  
321 M Elachour , M Hajji , M Salem , S Kertit , J Aride , R Coudert , E Essassi . *Corrosion-NACE* 1996. 52 (2)  
322 p. .
- 323 [El-Sherbiny ()] 'Some surfactants in the series of 2-(alkyldimethylammonio) alkanol bromides as inhibitors of  
324 the corrosion of iron in acid chloride solution'. E F El-Sherbiny . *Corros. Sci* 1999. 37 p. .
- 325 [Elachouri et al. ()] 'Some surfactants in the series of 2-(alkyldimethylammonio) solution'. M Elachouri , M S  
326 Hajji , M Salem , S Kertit , R Coudert , E M Essassi . *Corros.Sci* 1995. p. 37.
- 327 [Singh and Dey ()] 'Synergistic effects of inorganic and organic cations on inhibitive performance of propargyl  
328 alcohol on steel dissolution in boiling hydrochloric acid solution'. D N Singh , A K Dey . *Corrosion-NACE*  
329 1993. 49 p. .
- 330 [Zhao and Mu ()] 'The adsorption and corrosion inhibition of anion surfactants on aluminium surface in  
331 hydrochloric acid'. T P Zhao , G N Mu . *Corros. Sci* 1999. 41 p. .
- 332 [Abd El Rehim et al. ()] 'The corrosion inhibition study of sodium dodecyl benzene sulphonate to aluminium  
333 and its alloys in 1.0 M HCl solution'. S S Abd El Rehim , H H Hassan , M A Amin . *Mater. Chem. Phys*  
334 2003. 78 p. .
- 335 [Zucchi et al. ()] 'The influence of the chromium content on the inhibitive efficiency of some organic compounds'.  
336 F Zucchi , G Trabanelli , G Brunoro . *Corros.Sci* 1992. 33 p. .
- 337 [Bayol et al. ()] 'The inhibitive effect of hexamethylenetetramine on the acid corrosion of steel'. E Bayol , K  
338 Kayakirilmaz , M Erbil . *Mater. Chem. Phys* 2007. 104 p. .

- 
- 339 [Schweinsberg et al. ()] ‘The protective action of epoxy resins and curing agents-inhibitive effects on the aqueous  
340 acid corrosion of iron and steel’. D G Schweinsberg , A Nanayakkara , D Steiner . *Corros. Sci* 1988. 28 p. .
- 341 [Christopher ()] ‘The substituted 1, 3, 4-oxadiazoles: a new class of corrosion inhibitors of mild steel in acidic  
342 media’. M A B Christopher , AR . *Corros.Sci* 1994. 36 p. .
- 343 [Bentiss et al. ()] ‘The substituted 1, 3, 4-oxadiazoles: a new class of corrosion inhibitors of mild steel in acidic  
344 media’. F Bentiss , M Traisnel , M Lagrenee . *Corros. Sci* 2000. 42 p. .
- 345 [Maayta and Al-Rawashdeh ()] ‘The substituted 1, 3, 4-oxadiazoles: a new class of corrosion inhibitors of mild  
346 steel in acidic media’. A Maayta , N A Al-Rawashdeh . *Corros. Sci* 2004. 46 p. .
- 347 [Gece ()] ‘The use of quantum chemical methods in corrosion inhibitor studies’. G Gece . *Corros. Sci* 2008. 50  
348 p. .
- 349 [Raspini ()] ‘Time-to-corrosion initiation of chlorideexposed reinforced concrete considering time dependence of  
350 the diffusion coefficient’. I A Raspini . *Corrosion-NACE* 1993. 49 p. .
- 351 [Keddam and Takenouti ()] ‘Use of impedance measurements for the determination of the instant rate of metal  
352 corrosion’. M Keddam , H Takenouti . *J. Appl. Electrochem* 1972. 2 p. .
- 353 [Trabanelli ()] ‘Whitney Award Lecture: Inhibitors-An Old Remedy for a New Challenge inhibitors’. Trabanelli  
354 . *Corrosion* 1991. 1991. 47 p. .